WO 2004/018397 PCT/US2003/026331

## **CLAIMS**

What is claimed is:

1. A process for the preparation of 2-chloro-1,1,1,3,3,3-heptafluoropropane, comprising:

5

contacting a mixture comprising hydrogen fluoride, chlorine, and at least one starting material selected from the group consisting of halopropenes of the formula CX<sub>3</sub>CCI=CX<sub>2</sub> and halopropanes of the formula the CX<sub>3</sub>CCIYCX<sub>3</sub>, wherein each X is independently selected from the group consisting of F and Cl, and Y is selected from the group consisting of H, Cl and F, provided that the number of X and Y which are F totals no more than six, with a chlorofluorination catalyst in a reaction zone to produce a product mixture comprising CF<sub>3</sub>CCIFCF<sub>3</sub>, HCl, HF, and underfluorinated halogenated hydrocarbon intermediates;

15

20

10

wherein said chlorofluorination catalyst comprises at least one chromium-containing component selected from (i) a crystalline alpha-chromium oxide where at least 0.05 atom % of the chromium atoms in the alpha-chromium oxide lattice are replaced by nickel, trivalent cobalt or both nickel and trivalent cobalt, provided that no more than 2 atom % of the chromium atoms in the alpha-chromium oxide lattice are replaced by nickel and that the total amount of chromium atoms in the alpha-chromium oxide lattice that are replaced by nickel and trivalent cobalt is no more than 6 atom %, and (ii) a fluorinated crystalline oxide of (i).

25

- 2. The process of Claim 1 further comprising
  - (b) separating the product of step (a) to recover CF<sub>3</sub>CCIFCF<sub>3</sub>
    as a product and to obtain underfluorinated halogenated hydrocarbon intermediates; and

30

(c) returning underfluorinated halogenated hydrocarbon intermediates obtained in step (b) back to the step (a) reaction zone.

3. A process for the manufacture of a mixture of CF<sub>3</sub>CHFCF<sub>3</sub> and CF<sub>2</sub>=CFCF<sub>3</sub> by reacting a starting mixture comprising CF<sub>3</sub>CCIFCF<sub>3</sub> and hydrogen in the vapor phase at an elevated temperature, optionally in the presence of a hydrogenation catalyst, characterized by preparing the CF<sub>3</sub>CCIFCF<sub>3</sub> by the process of Claim 1.